Liquid Heating Systems

WORKSHOP IN

THE PRACTICAL ASPECTS OF

SOLAR SPACE AND DOMESTIC WATER HEATING SYSTEMS

FOR

RESIDENTIAL BUILDINGS

MODULE 9

LIQUID-HEATING SYSTEMS

SOLAR ENERGY APPLICATIONS LABORATORY

COLORADO STATE UNIVERSITY

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INTRODUCTION

Component selection is important for liquid-heating systems as it is for air-heating systems. The best components when assembled poorly or provided with an ineffective controller will yield poor system performance.

In a liquid-heating system heat from the collectors is generally always delivered to storage, and the heating load is always supplied from storage. An auxiliary heater is needed to provide heat when there is insufficient delivery rate of solar heat to meet the heating load. Such occasions can occur on excessively cold nights (or days) and after one or two successive cloudy days. The solar system should function automatically, provide the desired comfort level in the building at all times, require little maintenance and operate reliably over a long period of time.

OBJECTIVE

The objective of this module is to describe the interdependence of components of a liquid-heating system. The participants of the workshop should be able to:

- 1. Develop schematic and working plans of liquid solar systems,
- 2. Specify compatible system components
- 3. Identify all the system operating modes
- 4. Determine the size of system components
- Estimate the fraction of annual load that the solar system is expected to supply.

SYSTEM ARRANGEMENTS

DUAL-LIQUID SYSTEM

A recommended liquid-heating system in cold regions where freezing temperatures are dominant during the winter months is shown in Figure 9-1. The system is arranged to deliver solar heat first to storage and solar heat for space and domestic water are delivered from storage. When solar heat cannot provide the load requirements of either domestic water or space heating, auxiliary heating is then required. While the solar space heating system can be separated from the solar domestic hot water system, it is more convenient and economical to arrange an integrated system because during the warm months of the year the collectors can supply practically all of the domestic water heating that is needed.

SINGLE-LIQUID SYSTEM

An alternative system arrangement that is suitable for regions where the winter low temperatures are above the freezing point of water is shown in Figure 9-2. Water can then be circulated through the collector. While there are other liquids that could be used in the system, water is lowest in cost and has excellent thermo-physical properties.

COMPONENTS AND INTERACTIONS

COLLECTORS AND STORAGE

The efficiency of collectors in a solar system is influenced by all other components in the system. For maximum efficiency, the collector

PRESSURE RELIEF VALVE RADIATION COLLECTORS SOLAR AR DOMESTIC HOT WATER TANK TO BUILDING HOT WATER SYSTEM VENT AUXILIARY HEATER www. THERMAL HEAT EXCHANGER PRE-HEAT TANK STORAGE HOUSE FROM COLD WATER SUPPLY







should be supplied with liquid at the lowest available temperature. It follows therefore that liquid from the bottom of the storage tank should be circulated to the collector loop. If there is a heat exchanger in the circulation loop, as in Figure 9-1, the liquid is circulated from the bottom of the storage tank, through the heat exchanger and returned to the top of the storage tank. In a direct circulation loop, as in Figure 9-2, the liquid is taken from the bottom of storage and circulated through the collector. The heated liquid is then returned to the top of storage.

Storage temperatures are strongly influenced by the type and size of heat exchanger that is used to deliver heat to the load, and the type and size of heat exchanger used in the collector loop can influence the temperature of the liquid recirculated to the collector. The sizing of heat exchangers is therefore an important part of the system design. While oversizing the heat exchangers will have little influence on system performance, undersizing can seriously penalize the quantity of solar heat collection.

LOAD HEAT EXCHANGER

The temperature of water in storage is influenced by the type of load heat exchanger, and the arrangement of the auxiliary heater. The auxiliary heater can be placed in parallel with the solar storage tank as is shown in Figures 9-1 and 9-2, or in series with the solar storage tank to boost the temperature of the solar heated water. The parallel arrangement limits useful heating of space with solar heat in storage to a water temperature of about 90°F because at low temperatures, heat cannot be exchanged to the room air at a rate large enough to meet

load demands. In a series arrangement, auxiliary heat can be added to solar heat from storage, but the returning water temperature from the load heat exchanger can be higher than storage water temperature. When auxiliary heating is required frequently, as in the winter months, the series arrangement will result in auxiliary heating of the solar storage tank which in effect stores auxiliary energy. Use of auxiliary energy over the heating season is greater with the series arrangement than with the auxiliary heater in parallel.

AUXILIARY HEATER

The arrangement for auxiliary boosting shown in Figure 9-3 is preferable to either the parallel or series arrangement for minimizing auxiliary energy use. The capital and operating costs, however, are greater because an extra coil and circulation pump are required.



Figure 9-3. Solar Heating with Auxiliary Boosting

If a central air distribution system is provided in the building, the auxiliary warm air furnace in the arrangement shown in Figure 9-4 may be used effectively.



Figure 9-4. Solar Heating with Auxiliary Furnace

PUMPS AND OTHER EQUIPMENT

Centrifugal pumps should be used for circulating liquids in various loops of a solar system. With centrifugal pumps, pumping pressure is limited and if valves fail to open, or the pipeline becomes clogged, the danger of developing excessive pressures which could burst pipes is minimized. With known flow rate and system head losses, pumps may be selected from stock items in catalogs, or made to specifications by pump manufacturers. Impellers of stock item pumps may be trimmed to meet specifications. Centrifugal pumps should be located so that priming is not necessary, which could be a particular problem in a vented system or where a storage tank is located underground. Five feet of head on the suction side is sufficient to keep most pumps primed.

A check valve, micron filter, ion getter and an expansion tank should be installed in the collector loop as shown in Figure 9-5. The check valve prevents thermal cycling of the collector fluid when the pump is off and the collectors are colder than the building interior. A micron filter is recommended to remove particulate matter in the collector fluid. Particular attention is required at initial start-up because a large amount of foreign substances always seems to enter the pipes during installation. The filter should be changed immediately after initial operation, and changed as required thereafter.

The getter is simply a sacrificial anode to protect absorbers in collectors and pipes of disimilar metals in the system from galvanic corrosion. If the collector consists of aluminum absorbers, and the piping is copper, a getter may consist of aluminum window screen rolled up within a one-foot long neoprene hose and placed at the inlet to the collector manifold. The copper piping would terminate at one end of the neoprene hose and aluminum piping which joins the header would start at the other end.

An expansion tank is recommended to conserve the fluid in the collector when boiling occurs. The volume of the tank should be equal to the volume of fluid in the collectors and header, and should be positioned as close as possible to the top of the collector array. An open vent or pressure relief valve at the top of the tank will prevent pressure build up in the collector loop when boiling occurs.

Two connectors in the collector loop on the suction side of the pump are required to fill the collector loop with fluid, one is connected to the liquid source and the other to the same source to



Figure 9-5. Ancillary Devices in Collector Loop

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detect when filling is complete. If the filling connection is a few feet above the centrifugal pump, the filling operation will be facilitated. Drain and fill points should be suitably labeled.

Piping may consist of either copper or high temperature (CPVC) plastic pipe and all pipes should be insulated with appropriate material such as fiberglass pipe insulation at least one inch in thickness. Care should be taken to allow thermal expansion of the pipes and long pipe lengths should provide more freedom for expansion than short lengths. Pipes should be sized so that water velocity does not exceed five feet per second. In Table 9-1, recommended pipe diameters are indicated for flow rates in gallons per minute.

Table 9-1

Recommended Pipe Diameters for Various Flow Rates

Select Pipe Size	Gallons per Minute	Velocity FPS	Pressure Drop per 100 feet PSI
3/8	2	3.36	6.58
1/2	4	4.22	7.42
3/4	8	4.81	6.60
1	15	5.57	6.36
1-1/4	25	5.37	4.22

OPERATING CONTROLS

The fundamental operating modes of solar heating systems are collecting and storing solar heat and delivering heat from storage to load. The auxiliary unit must be controlled to provide heating when there is insufficient solar heat in storage to meet the demand.

A practical method for controlling the solar collection process involves use of temperature sensors which actuate the collector pump

(and also the storage circulation pump if a heat exchanger is used), whenever the temperature of the liquid leaving the collector exceeds the lowest temperature in storage by a preset amount, say 15°F. A sensor placed in the flow passage as close as possible to the collector exit, and a sensor near the bottom of the storage tank where storage water is likely to be coldest are compared electronically to preset temperatures to start and stop the circulation pumps. The temperature difference which shuts off the pumps is less than the temperature difference which starts the pumps, say 3°F, and the hysteresis in the temperature difference between on and off set points prevents cycling of the pumps at the beginning of the collection day and also at the end of the day.

When the liquid first circulates through the collectors at the beginning of the collection day, the temperature rise from inlet to the exit is only a few degrees because of the low solar intensity. Typically the temperature rise is 4 or 5°F. As the solar intensity increases, the temperature rise in the circulating liquid increases until by mid-day 15 to 20°F temperature rise occurs. During the circulation period, the storage water temperature increases gradually and by midafternoon when the solar intensity decreases, the collectors can no longer provide useful heat to storage and circulation stops.

The best control strategy to deliver heat to the building space is to use a room thermostat with a dual set point. Whenever the rooms require heat, the stage contact of the thermostat is completed and water from the storage tank is circulated to the load heat exchanger, regardless of storage tank temperature. If the storage water is warm enough, the room temperature rises, and the circulation system stops. The contact in the thermostat regulates the circulation pump and air blower.

If the storage water is not warm enough to deliver heat at a rate that is greater than the heat loss rate, the room temperature continues to fall until the second contact is made in the thermostat. The auxiliary water boiler or the auxiliary furnace is then activated to restore the room to the comfort temperature set at the thermostat. If the auxiliary water boiler is in series, only the auxiliary energy source is activated, but in a parallel arrangement a valve is also activated to direct heat flow from the auxiliary unit to the load heat exchanger. In an auxiliary arrangement, solar heat from storage continues to be utilized while auxiliary heating takes place until storage water reaches about 90°F. A low temperature over-ride switch t..en shuts off circulation of solar-heated water.

Solar preheating of domestic water is best regulated by a temperature difference comparator similar to the control of the collection ...op. The temperature sensor at the bottom of the solar storage tank may also be used for the DHW preheater loop control, and the difference in temperature between the bottom of the storage tank and top may be included in the temperature difference setting. Alternatively, a sensor may be installed at the top of the solar storage tank to control the preheater circulation pumps.

SYSTEM SIZING

There are various methods for determining the fraction of annual heating load supplied by solar systems as explained in Module 8. "Rules of Thumb" for sizing components of combined space and DHW systems and stand-alone DHW systems using liquids as the heat transfer fluid are given in Table 9-2. The detailed sizing procedure will

Table 9-2

Rules of Thumb for System Component Sizing

OLAR HYDRONIC HEATING/COOLING SYSTEMS					
Collector slope	Latitude + 15°				
Collector flow rate	~0.02 gpm/ft ² of collector				
Water storage size	1.5 to 2.5 gallons/ft ² of collector				
Pressure drop across collector	0.5 to 10 psi/collector module				
Collector heat exchanger	$F_{R}^{\prime}/F_{R}^{\prime}$ greater than 0.9				
Load heat exchanger	$\frac{\varepsilon_{L}C_{min}}{UA}$, greater than 1, less than 5				
SOLAR DOMESTIC HOT WATER HEATIN	IG SUBSYSTEMS				
Preheat tank size	1.5 to 2.0 times DHW auxiliary tank size				
Water-water heat exchanger	$arepsilon_{Hx}$, greater than 0.5, less than 0.8				

follow the f-chart method for liquid systems and the relative areas method described in Module 8. Additional explanations for f-chart application to liquid systems is explained in this section.

THE F-CHART METHOD

The basic approach to the f-chart method is explained in Module 8 and the f-chart for liquid-based systems is given in Figure 9-6. The coordinate axes, X and Y are defined by Equations (8-1) and (8-2). Corrections for Collector Heat Exchanger

When a heat exchanger is used between the collector and storage in a dual-liquid system, corrections to X and Y must be applied as follows:

X (new value) = X (from Eq. 8-1).
$$\frac{F_R}{F_R}$$
 (9-1)



Figure 9-6. f-Chart for Solar Liquid Heating Systems

where F'_R/F_R is the heat exchanger correction factor and depends on the heat exchanger effectiveness (See Module 7).

Y (new value) = Y (from Eq. 8-2)
$$\cdot \frac{F_R}{F_R}$$
 (9-2)

The new values of X and Y are used to estimate monthly solar fractions, s, from the chart.

Once the heat exchanger is selected and effectiveness $\epsilon_{\rm CS}$ is determined or calculated, the heat exchanger factor $F_{\rm R}^{\rm c}/F_{\rm R}$ for collector performance estimates can be determined from Figure 9-7.



Figure 9-7. Heat Exchanger Factor F'_R/F_R

The coordinates for the chart are determined as follows:

$$x = \frac{C_{c}}{\varepsilon_{cs} C_{min}}$$
(9-3)

in which

 C_c is the collector fluid heat capacity rate Btu/(hr·°F) ε_{cs} is the heat exchanger effectiveness, dimensionless C_{min} is the minimum of the collector or storage fluid capacitance ratio, Btu/(hr·°F)

and

$$y = \frac{A_{c}(F_{R}U_{L})}{C_{c}}$$
(9-4)

where

 A_c is the collector area, ft²

 $F_R {}^U L$ is the collector characteristic determined from the collector performance test data, as provided by the manufacturer, Btu/(hr·ft²·°F)

The heat exchange factor may also be calculated from Equation (9-5)

$$\frac{F_{\rm R}'}{F_{\rm R}} = \frac{1}{1 + y(x-1)}$$
(9-5)

EYAMPLE 9-1

Determine $F_R^\prime/F_R^{}$ for the collector array for the following conditions:

$$A_{c} = 500 \text{ ft}^{2}$$

$$F_{R}^{\tau\alpha} = 0.7$$

$$F_{R}U_{L} = 0.93 \frac{Btu}{hr \cdot ft^{2} \cdot {}^{\circ}F}$$

$$C_{c} = (\mathring{m} c_{p})_{c} = 10 \frac{gal}{min} \times 8.25 \frac{lb}{gal} \times .85 \frac{Btu}{16^{\circ}F} \times 60 \frac{min}{hr} = 4207 \frac{Btu}{hr^{\circ}F}$$

$$C_{s} = (\mathring{m} c_{p})_{s} = 20 \frac{gal}{min} \times 8.34 \frac{lb}{gal} \times 1 \frac{Btu}{lb^{\circ}F} \times 60 \frac{min}{hr} = 10008 \frac{Btu}{hr^{\circ}F}$$

$$\varepsilon_{cs} = 0.87 \text{ (From Module 7)}$$

The heat exchanger factor is determined as follows:

$$x = \frac{4207}{0.87(4207)} = 1.15$$
$$y = \frac{500(0.93)}{4207} = 0.111$$

From Figure 9-7, $F'_R/F_R \approx 0.98$ or from Equation (9-5),

$$F_{\rm R}^{\prime}/F_{\rm R} = \frac{1}{1 + (0.111)(1.15-1)} = 0.98$$

It should be noted that unless a very small or ineffective heat exchanger is used, the heat exchanger factor will generally be greater than 0.95.

Corrections for Storage Size

The nominal storage capacity for a liquid system is two gallons of water per square foot of collector. When storage sizes differ from the nominal size, corrections to the value of X should be made as follows:

X (corrected value) = X (from Eq. 8-1 or 9-1)
$$\cdot$$
 K₂ (9-6)

where ${\rm K}_{\rm 2}$ is determined from Figure 9-8.



Figure 9-8. Storage Capacitance Factor, K_2

Corrections for Load Heat Exchanger

One additional correction factor should be considered for a liquid-based system, which is the size of the load heat exchanger. A load heat exchanger that is small, will affect the storage tank temperature and consequently the temperature of the fluid to the collector. Hence, the system performance is affected. The correction factor is expressed as a function of the load heat exchanger effectiveness in comparison to the UA of the building, and is applied to Y as follows:

Y (corrected value) = Y (from Eq. 8-2 or 9-2) $\cdot K_4$ (9-7) where K_4 is determined from Figure 9-9.



Figure 9-9. Load Heat Exchanger Factor, K_4

Calculation Procedure

The procedure to be followed in the f-chart calculations are listed below:

- Step 1. List the data for the solar system by completing Worksheet A. Use available data from blueprints, specifications, inspections and handbooks. A heat load analysis for the building is required.
- Step 2. Determine the monthly and annual heating/DHW loads, L. Use Worksheet B. If the design heating load for the building is not available, an analysis is required.
- <u>Step 3</u>. Calculate the total monthly solar radiation, S. Use Worksheet C.
- <u>Step 4</u>. Determine the collector performance parameters, $F'_{R}(\tau \alpha)$, $F'_{R}U_{L}$. Use Worksheet D. Lines 1, 2, 3 and 4 are transferred from Worksheet A.

Corrections to $F_R(\tau\alpha)_n$, F_RU_L are necessary when the horizontal axis on the collector efficiency chart is based on fluid temperature other than the inlet temperature to the collector, T_i . Although collector test standards are suggested, efficiency curves are not presented in a uniform manner by the manufacturers. The corrections to $F_R(\tau\alpha)_n$, and F_RU_L for different cases are explained below.

Case 1. In
$$\frac{I^* - I_a}{I_T}$$
, T* is T_{in}. (fluid inlet temperature)
No correction is needed
T. + T

<u>Case 2</u>. If T* is $\frac{11}{2}$, which is the average of the inlet and outlet temperatures,

$$F_{R}(\tau\alpha)_{n}$$
 (new value) = $F_{R}(\tau\alpha)_{n}$ (from efficiency curve) $\cdot \left[\frac{1}{1 + \frac{F_{R}U_{L}A_{c}}{2C_{c}}}\right]$

where
$$C_c$$
 is heat capacitance rate of the collector fluid
 $(\dot{m} c_p)_c Btu/(hr \cdot rightarrow F)$
 $F_R U_L$ (new value) = $F_R U_L$ (from efficiency curve) $\cdot \left[\frac{1}{1 + \frac{F_R U_L A_c}{2 C_c}}\right]$
 $C_c = \dot{m} c_p = (volumetric) (fluid specific) (heat capacitance) (conversion) $\frac{Btu}{hr^r F}$$

$$\frac{\text{Case 3.}}{F_{R}(\tau\alpha)_{n}} = F_{R}(\tau\alpha)_{n} \text{ (from efficiency curve)} \cdot \left[\frac{1}{1 + \frac{F_{R}U_{L}A_{c}}{C_{c}}}\right]$$

$$F_{R}U_{L} = F_{R}U_{L} \text{ (from efficiency curve)} \cdot \left[\frac{1}{1 + \frac{F_{R}U_{L}A_{c}}{C_{c}}}\right]$$

Corrections to transmittance, τ , through the cover plates and absorptance, α , for the absorber plate are necessary because of sun angle variations on the collector during the day. The $F_R(\tau \alpha)_n$ determined for normal incidence during collector testing, must be corrected for an effective $F_R(\tau \alpha)$ for a day on a fixed-position collector.

$$\frac{F_R^{\tau\alpha}}{F_R(\tau\alpha)_n} = \{ \begin{array}{l} 0.91 \text{ for two cover plates} \\ 0.93 \text{ for one cover plate} \end{array} \right.$$

<u>Step 5.</u> Determine correction factors K₂ and K₄. Use Worksheet E.
 <u>Step 6.</u> Calculate system performance parameters. Use Worksheet F.
 <u>Step 7.</u> Determine system performance factors f (monthly) and F (annual). Use Worksheet G.

EXAMPLE 9-2

Design a solar heating and hot water system for a three bedroom house located in Fort Collins, Colorado. The house is wood framed with R-13 wall insulation and R-19 ceiling insulation. The overall dimensions of the house are 27 feet wide and 55 feet long, with a usable roof area of 954 ft², measuring 18 by 53 feet.

The heat loss calculations for the building have been made, and the overall UA (heat conductance) is 714 $Btu/(hr \cdot F)$. Using the time conversion from hour to day, the heating load for the building is 17,136 Btu/DD. Complete Worksheets A through G.

<u>Answer</u>. For collector area of 500 ft², the liquid-heating system will provide 68 percent of the total annual space and DHW heating load.

(Text continues on page 9-31)

LIQUID SYSTEMS

Worksheet A Sheet 1 of 2

SOLAR SYSTEM DATA

Building Owner Mr + Mrs John Sunbody 736 Sunshine Ave Address Fort Collins Co Ph. 482-0000 Contractor Solar Construction Co Ph. 482-0001 Type of System (liquid or air, H/DHW Liquid , H/DHW Site and Building Data 1. Location: Nearest City Fort CollinsLatitude 40.6°N Btu/(hr•°F) 2. Building UA 714 80 gallons/day DHW volume per day 3. Collector manufacturer Honey well - Lennox 4. ft² 5. Collector area 500 50 degrees 6. Collector tilt 7. Tilt = latitude + 10 degrees from south Collector orientation _____ degrees 8. % in December ()9. Collector shading Collector efficiency data 10. (a) $F_{R}(\tau \alpha)_{n}$. 54 Btu/(hr.ft².°F) (b) F_pU₁ (c) Fluid temperature basis (circle one) Ti Case 1 $\frac{T_i + T_{out}}{2}$ Case 2 Tout Case 3 11. Collector Fluid: (a) Composition: water-ethylene glycol, 30% 0.90 Btu/(1b.°F) (b) Specific heat, c_p 8.92 1b/gal or 1b/ft³ (c) Specific weight γ 0 gal/min or ft³/min (d) Flow rate G Storage Data water 12. Storage medium $\int \frac{1}{5} \frac{$ 13. Unit volume 150 gal or ft³ 14. Total volume (item 5 x 13)

Sheet 2 of 2 LIQUID SYSTEMS 15. Specific heat of storage material c_n Btu/(1b.°F) √. 34 lb/gal or lb/ft³ 16. Specific weight 17. Total mass (14 x 16) M 1b. 18. Total heat capacity (17 x 15) 62.55 Btu/°F $C_s = Mc_p$ 19. Total heat capacity per unit 12.5 Btu/(ft^{2.°}F) collector area $(18 \div 5)$ Heat Exchangers Counter Flow and Collector/storage type 20. Young Radiator manufacturer 15 gal/min, ft³/min 21. Storage loop flow rate 22. Heat exchange effectiveness ε_{cs} $\cancel{0.75}$ 23. Load heat exchanger type Cross - Flow, water air and Radiator Young manufacturer 24. Load loop flow rate __gal/min 1200 ft³/min Building air supply flow rate 25. 26. Heat exchange effectiveness ε_1 DHW Preheater 27. Collector/storage heat exchanger type <u>(ounterflow</u> and Young Reliator manufacturer gal/min, ft³/min 28. Collector loop flow rate 29. Heat exchanger effectiveness ε_{Hw} 0.7 80 gal Storage volume 30. 667 1b Storage mass, M_{St} (line 30 x 8.34) 31. Auxiliary Furnace/Boiler Boiler 00 32. Type Lennox 33. Manufacturer 100, 600 Btu/hr 34. Rated capacity electricit 35. Auxiliary energy source Auxiliary DHW Unit gal 36. Size lectric 37. Auxiliary energy source Hot water set temperature 38.

Worksheet A

Worksheet B LIQUID SYSTEMS

HEATING AND/OR DOMESTIC HOT WATER LOAD, L

1	1	1			· · · · · · · · · · · · · · · · · · ·	1	1	
	1	2		3	4	5	6	7
Month	Monthly Degree Days DD °F∙days	Monthly Space Htg Load Q _s Btu/Mo.	No. of Days/ Mo. N	Vol. of DHW Used/Mo. Gal./Mo.	Temp. Water Main Sup. T _m °F	DHW Temp. Rise T _{HW} -T _m °F	Monthly DHW Load Q _W Btu/Mo.	Total Heating Load L Btu/Mo.
Jan.	1138	x 106 19.4	31	2480	39	101	x 106 2.1	21.5
Feb.	938	16.1	28	2240	40	100	1.9	18.0
March	881	15.2	31	2480	43	97	2.0	17.2
April	558	9.6	30	2400	49	91	1.8	11.4
May	288	5.0	31	2480	55	85	1.8	6.8
June	66		30	24-00	60	80	1.6	2.7
July	6	. (31	2480	63	. 77	1.6	1.7
Aug.	9	.2	31	2480	64	76	1.6	1.8
Sept.	117	2.0	30	2400	63	77	1.5	3.5
Oct.	428	7.3	31	24-80	56	84	1.7	9.0
Nov.	819	14.0	3D	2400	45	95	1.9	15.9
Dec.	1035	17.7	31	2480	37	103	2.1	14-8
				8		Total	21.0	129.3

Project <u>Sunbody</u> Residence

 $Q_d = 51, 410$ Btu/h (Given data or calculate

as in Module 3)

$$DTD = 70 - T_0$$

= 70 - (-2) = 72.

Where: $T_0 = 99\%$ winter design temperature. (From ASHRAE Fundamentals, or Table 3-2)

70°F = indoor design

$$UA = \frac{Q_d}{DTD} = 714 \quad 8 \pm u / (hr \cdot \circ F)$$

 $T_{HW} = 140^{\circ} F$

1. From Table 3-2 or Figures 3-2 through 3-13 2. $Q_s = (24)(UA)(Degree Day)$

3. (Vol/day)x(no. days/mo.) = <u>\$0</u> (gal./day)x(no. days/mo.)

6. $Q_w = (vol. of water) \times 8.34 \times 1 \times (T_{HW}-T_m)$.

7. $L = Q_{s} + Q_{w}$

TOTAL MONTHLY SOLAR RADIATION AVAILABLE, S

Project	Syn bod	y Residence	
Location	Fort	Collins	
Collector Tilt	Lat	+15°	
Nearest Data Site	в	oulder	_

and the second	and the least of the	2	3
Month	Monthly Avg. Daily Rad. on Tilt Surf. T Btu/(Day•ft ²)	No. of Days in month N	Tot. Monthly Radiation on Tilt Surf. S Btu/(Mo•ft ²)
Jan.	1439	31	44,609
Feb.	1533	· 28	4-2,924
March	1409	31	59,179
April	1663	30	49,890
May	1425	31	44,175
June	1491	30	44,730
July	1535	31	47,585
Aug.	1458	31	45, 198
Sept.	1702	30	51,060
Oct.	1659	31	51,429
Nov.	1507	30	4-5,210
Dec.	14-18	31	43,958

[1] From Table 5-5 for Colorado cities

[3] Column [1] x Column [2]

Worksheet D Sheet 1 of 2 LIQUID SYSTEMS

COLLECTOR COMBINED PERFORMANCE CHARACTERISTICS, $F'_{R}(\tau \alpha) \cdot F'_{R}U_{I}$ PROJECT Sunbody Residence Collector Efficiency Data from Worksheet A (lines 10(a), (b)) = 0.73 Intercept, $F_{R}(\tau \alpha)_{n}$ 1. = 0,541. (t_{in}) 2. $\frac{t_{in} + t_{out}}{2}$, Slope, F_pU 2. Reference Temperature Basis: Collector area, A 500 ft² 3. 4. Collector volumetric flow rate (Worksheet A, 11(d)) 10 ____gal/min or ft³/min Correction to t_{in} basis 5. Case 1: (no correction) $F_R(\tau \alpha)_n = 0.73$ $F_{\rm R} U_{\rm L} = 0.54$ 6. Case 2: $F_R(\tau \alpha)_n = F_R \tau \alpha \times \left[\frac{1}{1 + \frac{F_R U_L A_C}{2 C}}\right] =$ $F_{R}U_{L} = F_{R}U_{L} \times \left[\frac{1}{1 + \frac{F_{R}U_{L}A_{c}}{2C}}\right] = C_{c} = \dot{m}c_{p} = (volumetric)(density)(time)(conversion)(specific)(heat)$ = 10x 8.92 x 60x 0.90 = 4817 Btu/(hr. °F) for liquids, density - (8.34 lb/gal) x where: (specific) for air, density = 0.075 lb/ft³ at 70° and 1 atm. specific heat = 0.24 Btu/lb.°F 7. Case 3: $F_R(\tau\alpha)_n = F_R(\tau\alpha)_n \times \left[\frac{1}{1 + \frac{F_R U_L A_C}{C_n}}\right] =$ $F_R U_L = F_R U_L \times \left[\frac{1}{1 + \frac{F_R U_L A_c}{1 +$ Incident Angle Modifier, $\frac{F_R(\tau\alpha)}{F_R(\tau\alpha)_n} = \{ \begin{array}{c} 91 \\ 93 \end{array} \}$ for two cover plates 8.

Worksheet D Sheet 2 of 2 LIQUID SYSTEMS

Collector Loop Heat Exchanger Modifier, $\frac{F_R^{\prime}}{F_P}$

9. For air systems and liquid systems without a collector/storage heat exchanger, $\frac{F_{R}^{2}}{F_{R}} = 1$ Capacitance Rate:

10. $C_c = (\text{from line 6}) = \frac{4817}{7506} \text{Btu/(hr.°F)}$ 11. $C_s = (\text{calc. as for } C_c \text{ above}) = \frac{7506}{7506} \text{Btu/(hr.°F)}$ 12. $C_{\text{min}} = (\text{lesser of } C_c \text{ of } C_s) = \frac{4817}{7506} \text{Btu/(hr.°F)}$

13. Collector Storage Heat Exchanger Effectiveness,
$$\varepsilon_{cs} = 0.15$$

14.
$$x = \frac{C_c}{\varepsilon_{cs} C_{min}} = \frac{48[1/0.15(4817)}{(\text{from Worksheet A, line 22})} = \frac{1.33}{1.33}$$

15.
$$y = \frac{A_c(F_R U_L)}{C_c} = \frac{500(.54)/4817}{-0.56} = \frac{.056}{.056}$$

16.
$$\frac{F_R}{F_R}$$
 = from Figure 9-7 or = $\frac{1}{1 + y(x-1)}$ = _____, 98

17.
$$F_{R}^{i}(\tau \alpha) = F_{R}(\tau \alpha)_{n} \times \frac{(\tau \alpha)}{(\tau \alpha)_{n}} \times \frac{F_{R}^{i}}{F_{R}} = \frac{(0.73)(.93)(.93)(.98)}{(.98)} = .67$$

18. $F_{R}^{i}U_{L} = F_{R}U_{L} \times \frac{F_{R}^{i}}{F_{P}} = \frac{(.54)(.98)}{(.98)} = .53$

CORRECTION FACTORS, K_2 , K_4

PROJECT Sumbody Residence
Storage Mass Capacitance Factor K₂
Note: M includes hot water sotrage volume where it is solar
heated
1. gals/ft² of collector 1.5
2. K₂ = (from Figure 9-8) = 1.07
Load Heat Exchange Factor, K₄
3.
$$\epsilon_L$$
 (from Worksheet A, line 26) = 0.75
4. $C_{hot water supply loop = mc_p = C_H$
(from Worksheet A, lines 24 x 8.25 x 60) = 6005 Btu/(hr·ft²)
5. $C_{air \ loop} = mc_p = C_A$
(from Worksheet A, line 25 x 0.075 x .24 x 60) = 1246 Btu/(hr·ft²)
6. $C_{min} = smaller \ of C_H \ or C_A = 1246 Btu/(hr·ft2)
7. (UA) bldg = (from Worksheet A, or B) = 114 Btu/(hr·°F)
8. $\frac{\epsilon_L \ C_{min}}{UA} = \frac{0.977}{0.977}$$

Worksheet F LIQUID SYSTEMS

SYSTEM PERFORMANCE PARAMETERS X, Y

PROJECT Sunbody Residence

	ĩ	2	3	4	5	6 .	7	8
Month	Tot. Monthly Radiation on Tilt Surf. S Btw/(Mo.ft ²)	Total Heating Load L	5/1	۲ ۲- ۱۹	Mo. Av. Temp. Ta F	212-T °F ^a	Tot. Hrs in Mo. ∆ time	Y
lan		x 106	00101	(12	0.9	164	7//	1 61
	44,609	21.5	. 00201	.615	20	109-	/ + +	1.01
Feb.	42,924	18.0	.00238	.774	32	180	672	1-91
March	59,119	11.2	.00 344	1.118	36	176	744	2.16
April	49,890	11.4	. 00438	1.424	46	166	720	2.97
May	44,175	6.8	.00650	2.111	56	156	744	4.84
June	44,730	2.7	.0166	5.385	63	149	720	11.27
July	47,585	1.7	. 0280	9.097	65	141	744	18.25
Aug.	45, 198	1.8	.0251	8.161	65	197	744	17.23
Sept.	51,060	3.5	.0 146	4.742	61	151	720	8.81
Oct.	51,429	9.0	.00 571	1.856	5	161	744	3.77
Nov.	45,210	15.9	.00284	.123	38	174	720	2.23
Dec.	43,958	19.8	.00222	.722	32	180	744	1.92
1. From Workshe 2. From Workshe 4. $Y = \frac{A_c F_R'(\tau \alpha)}{L}$ 5. From Table 5 8. $X = \frac{A_c F_R'U_L(1)}{E}$ $= F_2 \cdot \{[6]\}$	eet C, Col. 3 eet B, Col. 7)S - x K ₄ = F ₁ · $\frac{S}{L}$ 5-5 $\frac{\Gamma_{ref}-T_a)\Delta time}{L}$ x K ₂ \cdot [7]}÷[2]			A _c F _R ^{τα} F _R U _L K ₁ K ₂ F ₁ =	= = = = Α _c F ¹ _b τα Κ _A		<u>500</u> f .67 (.53 (1.0 (1.07 (.97 (325	t ² Wksht D) Wksht D) Wksht E) Wksht E) Wksht E)
	olumns			$F_2 = 1$	$A_c F_R^U K_2 =$		283-6	

1

SOLAR FRACTION FOR DIFFERENT COLLECTOR SIZES

In Example 9-2, the detailed calculations yielded the result that solar energy, with 500 ft² of Honeywell-Lennox collectors and compatible system components, provide 68 percent of the total annual space and domestic hot water heating load for the building. To determine the annual solar fraction provided by a system with different collector areas, the f-chart used for the computations with 500 ft² of collectors, and only worksheet G are needed. It is not necessary to rework the entire calculation procedure from worksheet A through worksheet G.

As an example, the monthly and annual solar fractions for 300 ft^2 of collectors can be determined by following the procedure below:

Step 1. - Calculate the area ratio (new area/old area)

In this example 300/500 = 0.6

Step 2. - For each month multiply the f-chart parameters X and Y
 (Columns 2 and 3, Worksheet G) by the area ratio.

Step 3. - Use the f-chart (Figure 9-6) and determine the new solar fractions for each month.

Step 4. - Complete a new worksheet G and determine the annual fraction, F.

The procedure described above is followed and results are shown on the new worksheet G.. With 300 ft^2 of liquid-heating collectors, the system will provide 49 percent of the annual space and DHW heating load.

Worksheet G LIQUID SYSTEMS

FRACTION OF TOTAL HEATING LOAD SUPPLIED BY SOLAR ENERGY, FAnnual PROJECT Sun body Residence.

COLLECTOR AREA 300 ft2

	1 2 2	2	3	4	1 5
Month	Tot. Mo. Htg. Load L Btu/mo.	System Parameters X	System Parameters Y	Solar Fraction/ mo. f	Actual Solar en/mo E Btu/mo.
Jan.	21.5	1.09	. 40	0.31	6.7
Feb.	18.0	1.15	.46	0.36	6.5
March	17.2	1.30	. 67	0.50	8.6
April	11.4	1.78	. 85	0.60	6.8
May	6.8	2.90	1.27	0.79	5.4
June	2.7	6.76	3.23	1.0	2.7
July	1.7	10.95	5.46	1.0	1.7
Aug.	1.8	10.34	4.90	1.0	1.8
Sept.	3.5	5.29	2.84	1.0	3.5
Oct.	9.0	2-26	1.12	0.14	6.7
Nov.	15.9	1.34	. 55	0.42	6.7
Dec.	19.8	1.15	.43	0.33	6.5

L_{tot} =

E_{tot} =

E tot F_{Annual} tot

- From Worksheet B 1.

- From Worksheet F, Column 9
 From Worksheet F, Column 4
 From "f chart", Figure 9-6
 E = f x L

THE RELATIVE AREAS METHOD

The annual solar fraction for the solar system of Example 9-2 is calculated using the relative areas method described in Module 8.

EXAMPLE 9-3

Determine the annual solar fraction for the solar system of Example 11-2, using the relative areas method, first for 500 ft², then for 300 ft², using the values in Table 11-6 for Denver, Colorado.

For convenience, use the worksheet for the relative areas method:

Answer.

 $F = 0.73 \text{ for } A_{c} = 500 \text{ ft}^{2}$ $F = 0.58 \text{ for } A_{c} = 300 \text{ ft}^{2}$ From the f-chart method the results were $F = 0.68 \text{ for } A_{c} = 500 \text{ ft}^{2}$ $F = 0.49 \text{ for } A_{c} = 300 \text{ ft}^{2}$

SOLAR SYSTEM DATA

Building Owner Mrt Mrs John Sunbody Address 736 Sunshine Ave Colo Ph. 482-0000 contractor Solar Construction Ph. 482-0001 Type of System (liquid, air, H/DHW, DWH) Liquid H/DHW Site and Building Data Location: Nearest City Fort Collins Latitude 40.6°N 1. 714 Building UA Btu/(hr.°F) 2. 80 gallons/day 3. DHW volume per day Collector Data 4. Collector manufacturer Lennox5. Collector Area, $A_c = 500$ ____2 Collector efficiency data from manufacturer's information: 6. 0.73 (a) F_p(τα) 0.54 Btu/(hr·ft²·°F) (b) $F_{D}U_{I}$ Correction for fluid temperature basis 7. (a) Case 1: (no correction) (i) $F_{R}(\tau \alpha)_{n} = F_{R}\tau \alpha$ (from line 6) <u>0.73</u> (ii) $F_R U_L = F_R U_L$ (from line 6) O.54 Btu/(hr·ft²·°F) (b) Case 2: $\frac{T_{in} + T_{out}}{2}$ (correction needed) $C_{c} = (\dot{m}c_{p})_{c} = (\frac{Vol flow}{rate})(density)(\frac{time}{conversion})(\frac{specific}{heat})$ $= \frac{10}{\min} \times \frac{gal}{gal} \times \frac{g.92}{gal} \times 60 \frac{\min}{hr} \times \frac{0.9}{lb \cdot {}^{\circ}F}$ 4817 Btu/(hr.°F)

Correction Factor =
$$\left[\frac{1}{1 + \frac{F_R U_L A_C}{2C_C}}\right] = \frac{1}{1 + \frac{F_R U_L A_C}{2C_C}}$$

(1) $F_R(\tau \alpha)_n = F_R \tau \alpha(\text{from line 6a}) \times (\text{correction factor})$
 $= \frac{1}{1 + \frac{F_R U_L}{2C_C}} = \frac{1}{1 + \frac{F_R U_L A_C}{C_C}}$
(1) $F_R U_L = F_R U_L (\text{from line 6b}) \times (\text{correction factor})$
 $= \frac{1}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6a}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}}$
(1) $F_R (\tau \alpha)_n = F_R (\tau \alpha) (\text{from line 6a}) \times (\text{correction factor})$
 $= \frac{1}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 6b}) \times (\text{correction factor})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L (\text{from line 7b})}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R U_L A_C}{1 + \frac{F_R U_L A_C}{C_C}} = \frac{F_R$

Corrections to Collector Parameters

10. Incident angle modifier

(a)
$$F_R(\tau \alpha) = F_R(\tau \alpha)_n \times 0.91$$
 (for two cover plates)

= _____ x 0.91 = _____

(b) $F_R(\overline{\tau\alpha}) = F_R(\tau\alpha)_n \times 0.93$ (for one cover plate)

List c_1 , c_2 , A_S , A_D , Z from Table 11-5

12.
$$A_s \text{ or } A_D = ... 191 \quad z = ... 291 \quad c_1 = ... 531 \quad c_2 = ... 301$$

For Solar Heating and DHW Systems:

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- 4. Climate Atlas of the United States, U.S. Department of Commerce NOAA, National Climatic Center, Federal Building, Asheville, N.C. 28801.
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Worksheet A Sheet 1 of 2 LIQUID SYSTEMS

SOLAR SYSTEM DATA

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Building (Owner			
Address			Ph	
Contracto	r	Ph		
Type of S	ystem (liquid or air, H/D	HW		
Site and	Building Data			
1.	Location: Nearest City_		Lati	tude
2.	Building UA			_Btu/(hr·°F)
3.	DHW volume per day			_gallons/day
4.	Collector manufacturer	<u></u>		
5.	Collector area			_ft ²
6.	Collector tilt			_degrees
7.	Tilt = latitude +			degrees
8.	Collector orientation	degrees		_from south
9.	Collector shading			_% in December
10.	Collector efficiency dat	ta		
	(a) F _R (τα) _n			_
	(b) F _R UL			_ Btu/(hr•ft ² •°F)
	(c) Fluid temperature ba	asis (circle on	e)	
	Case 1	T.		
	Case 2	$\frac{T_i + T_{out}}{2}$		
	Case 3	Tout		
11.	Collector Fluid:			
	(a) Composition:			
	(b) Specific heat, c _p			Btu/(lb•°F)
	(c) Specific weight γ	Record of the		_lb/gal or lb/ft ³
	(d) Flow rate G			_gal/min or ft ³ /min
Storage [Data			
12.	Storage medium			
13.	Unit volume			gal/ft ² or ft ³ /ft ²
14.	Total volume (item 5 x	13)	<u></u>	gal or ft ³

			Worksheet A Sheet 2 of 2 LIQUID SYSTEMS
	15.	Specific heat of storage material c _n	Btu/(lb.°F)
	16.	Specific weight	lb/gal or lb/ft ³
	17.	Total mass (14 x 16) M	1b.
	18.	Total heat capacity (17 x 15) C _s = Mc _p	Btu/°F
	19.	Total heat capacity per unit collector area (18 ÷ 5)	Btu/(ft².°F)
Heat	Excha	angers	
	20.	Collector/storage type	and
		manufacturer	
	21.	Storage loop flow rate	gal/min, ft ³ /min
	22.	Heat exchange effectiveness e_{cs}	
	23.	Load heat exchanger type	and
		manufacturer	
	24.	Load loop flow rate	gal/min
	25.	Building air supply flow rate	ft ³ /min
	26.	Heat exchange effectiveness ϵ_L	
DHW I	Prehea	ater	
	27.	Collector/storage heat exchanger type manufacturer	and
	28.	Collector loop flow rate	gal/min, ft ³ /min
	29.	Heat exchanger effectiveness $\varepsilon_{H_{\rm eff}}$	
	30.	Storage volume	gal
	31.	Storage mass, M _{S+} (line 30 x 8.34)	15
Auxi	liary	Furnace/Boiler	
	32.	Nanufacturer	
	33. 24	Pated capacity	Btu/br
	34.	Auxiliany onongy source	b cu/ m
	55.	Auxillary energy source	
Auxi	liary	DHW Unit	
	36.	Size	gal
	37.	Auxiliary energy source	
	38.	Hot water set temperature	^V F

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	1	2	-	3	4	5	6	7
Month	Monthly Degree Days DD °F∙days	Monthly Space Htg Load Q _s Btu/Mo.	No. of Days/ Mo. N	Vol. of DHW Used/Mo. Gal./Mo.	Temp. Water Main Sup. T _m °F	DHW Temp. Rise T _{HW} -T _m °F	Monthly DHW Load Q _W Btu/Mo.	Total Heating Load L Btu/Mo.
Jan.			31					
Feb.			28					
March			31					
April			30					
May			31					
June			30			-		
July			31					
Aug.			31					
Sept.			30					
Oct.			31					
Nov.			30					
Dec.			31					
						Total		

HEATING AND/OR DOMESTIC HOT WATER LOAD, L

1. From Table 3-2 or Figures 3-2 through 3-13 2. $Q_s = (24)(UA)(Degree Day)$

3. (Vol/day)x(no. days/mo.) =4. From Table 8-3 for selected cities 6. $Q_w = (vol. of water) \times 8.34 \times 1 \times (T_{HW}-T_m)$. _(gal./day)x(no. days/mo.)

7. $L = Q_{S} + Q_{W}$

Btu/h $Q_d =$ (Given data or calculate as in Module 3) $DTD = 70 - T_0$

Project _____

= 70 - _ _ =

Where: $T_0 = 99\%$ winter design temperature.

(From ASHRAE Fundamentals, or Table 3-2)

70°F ≈ indoor design

 $UA = \frac{Q_d}{DTD} =$

T_{HW} =

TOTAL MONTHLY SOLAR RADIATION AVAILABLE, S

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Project
Location
Collector Tilt
Nearest Data Site

	1	2	3
Month	Monthly Avg. Daily Rad. on Ti <u>l</u> t Surf. ^I T Btu/(Day•ft ²)	No. of Cays in month N	Tot. Monthly Radiation on Tilt Surf. S Btu/(Mo•ft ²)
Jan.		31	
Feb.		28	
March		31	
April		30	
May		31	
June		30	
July		31	
Aug.		31	
Sept.		30	
Oct.		31	
Nov.		30	
Dec.		31	

[1] From Table 5-5 for Colorado cities

[3] Column [1] x Column [2]

Worksheet D Sheet 1 of 2 LIQUID SYSTEMS



Collector Loop Heat Exchanger Modifier, $\frac{F_R^{i}}{F_P}$

9. For air systems and liquid systems without a collector/storage heat exchanger, $\frac{F_R'}{F_R} = 1$ Capacitance Rate:

10.
$$C_c = (\text{from line 6}) = _____Btu/(hr \cdot F)$$

- 11. $C_s = (calc. as for C_c above) = _____ Btu/(hr·°F)$ 12. $C_{min} = (lesser of C_c of C_s) = _____ Btu/(hr·°F)$
- 13. Collector Storage Heat Exchanger Effectiveness, $\epsilon_{cs} =$

14.
$$x = \frac{C_c}{\varepsilon_{cs} C_{min}} = \frac{14}{(\text{from Worksheet A, line 22})} = \frac{14}{(\text{from Worksheet A, line 22})}$$

17.
$$F_{R}^{i}(\overline{\tau \alpha}) = F_{R}(\tau \alpha)_{n} \times \frac{(\overline{\tau \alpha})}{(\tau \alpha)_{n}} \times \frac{F_{R}^{i}}{F_{R}} =$$

18. $F_{R}^{i}U_{L} = F_{R}U_{L} \times \frac{F_{R}^{i}}{F_{R}} =$

CORRECTION FACTORS, K_2 , K_4

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	PROJECT		
Storage M	ass Capacitance Factor K ₂		
Note	: M includes hot water sotrage volume wh heated	ere it is so	lar
1.	gals/ft ² of collector		
2.	K ₂ = (from Figure 9-8) =	<u></u>	
Load Heat	Exchange Factor, K ₄		
3.	ϵ_{L} (from Worksheet A, line 26) =		
4.	C _{hot water supply loop} = mc _p = C _H (from Worksheet A, lines 24 x 8.25 x 60)	=	
			Btu/(hr•ft ²)
5.	$C_{air loop} = mc_p = C_A$ (from Worksheet A, line 25 x 0.075 x .24	x 60) =	
			Btu/(hr•ft ²)
6.	C _{min} = smaller of C _H or C _A =		Btu/(hr•ft ²)
7.	(UA) bldg = (from Worksheet A, or B) =		
			Btu/(hr.°F)
8.	$\frac{\varepsilon_{L} \ \text{Umin}}{\text{UA}} =$		
9.	K ₄ = (from Figure 9-9) =		

SYSTEM PERFORMANCE PARAMETERS X, Y

PROJECT

			a state of the sta					
	1	2	3	4	5	6	7	8
Month	Tot. Monthly Radiation on Tilt Surf. S Btu/(Mo•ft ²)	Total Heating Load L Btu/Mo.	S/L	Y F ₁ •[3]	Mo. Av. Temp. T _a °F	212-T °F ^a	Tot. Hrs in Mo. ∆ time hr.	X
Jan.							744	
Feb.							672	
March							744	
April					· · · · · · · · · · · · · · · · · · ·		720	
May							744	
June							720	
July							744	
Aug.							744	
Sept.							720	
Oct.							744	
Nov.							720	
Dec.					2		744	
1. From Worksh 2. From Worksh 4. $\gamma = \frac{A_c F_R'(\tau \alpha)}{L}$ 5. From Table 8. $\chi = \frac{A_c F_R'U_L}{L}$ $= F_2 \cdot \{[6]\}$	the et C, Col. 3 the et B, Col. 7 $\frac{S}{-x} K_4 = F_1 \cdot \frac{S}{L}$ $\frac{T_{ref} - T_a \Delta time}{L} x K_2$ $\cdot [7] \cdot [2]$ olumns			A_{c} $F_{R}^{T\alpha}$ $F_{R}^{T\alpha}$ F_{R}^{U} K_{1} K_{2} K_{4} $F_{1} = A$ $F_{1} = A$	$=$ $=$ $=$ $=$ $=$ $A_{c}F_{R}^{i} \overline{\tau \alpha} K_{4}^{i}$		f (((t ² Wksht D) Wksht D) Wksht E) Wksht E) Wksht E)

Worksheet G LIQUID SYSTEMS

FRACTION OF TOTAL HEATING LOAD SUPPLIED BY SOLAR ENERGY, FAnnual PROJECT 2 3 5 COLLECTOR AREA ft² 4 Actual Tot. Mo. System System Solar Solar Month Parameters Htg. Load Parameters Fraction/ en/mo L Х Y E mo. Btu/mo. f Btu/mo. Jan. Feb. March April May June July Aug. Sept. Oct. Nov. Dec.

L_{tot} =

E_{tot} =

Etot = ____ = ___ FAnnual = tot

1. From Worksheet B

- 2. From Worksheet F, Column 9
- From Worksheet F, Column 4
 From "f chart", Figure 9-6
 E = f x L

Relative Areas Method Worksheets Sheet 1 of 3

SOLAR SYSTEM DATA

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Building ()wner	
Address		Ph
Contracto		Ph
Type of S	/stem (liquid, air, H/DHW, DWH)	
Site and	Building Data	
1. 2. 3.	Location: Nearest City Building UA DHW volume per day	Latitude Btu/(hr•°F) gallons/day
Collector	Data	
4. 5. 6.	Collector manufacturer Collector Area, $A_c =Collector efficiency data from manufacturer's(a) F_R(\tau \alpha)$	ft ² information:
	(b) F _R U ₁	_Btu/(hr•ft ² •°F)
7.	Correction for fluid temperature basis (a) Case 1: (no correction)	
	(i) $F_R(\tau \alpha)_n = F_R \tau \alpha$ (from line 6) (ii) $F_R U_L = F_R U_L$ (from line 6)	
	(b) Case 2: $\frac{T_{in} + T_{out}}{2}$ (correction needed)	
	C _c = (mc _p) _c = (^{Vol flow})(density)(time (specific) conversion heat
	= <u>gal</u> x <u>lb</u> x 60 <u>min</u> min x <u></u> gal x 60 <u>hr</u>	x <u>Btu</u> Ib•°F
		Btu/(hr·°F)

Correction Factor =
$$\begin{bmatrix} 1 \\ 1 + \frac{F_R U_L A_C}{2C_C} \end{bmatrix}$$
 = _______
(i) $F_R(\tau \alpha)_n = F_R \tau \alpha (\text{from line 6a}) \times (\text{correction factor})$
 $= _ _ _ X _ _ = _ _$
(ii) $F_R U_L = F_R U_L (\text{from line 6b}) \times (\text{correction factor})$
 $= _ _ _ Btu/(hr \cdot ft^2 \cdot \circ F)$
(c) Case 2: $T_{out}(\text{correction needed})$
Correction Factor = $\frac{1}{1 + \frac{F_R U_L A_C}{-C_C}}$
(i) $F_R(\tau \alpha)_n = F_R(\tau \alpha)(\text{from line 6a}) \times (\text{correction factor})$
 $= _ _ X _ _ = _$
(ii) $F_R U_L (\text{from line 6b}) \times (\text{correction factor})$
 $= _ _ X _ _ = _$
(ii) $F_R U_L (\text{from line 6b}) \times (\text{correction factor})$
 $= _ _ X _ _ = _$
(ii) $F_R U_L (\text{from line 6b}) \times (\text{correction factor})$
 $= _ _ X _ _ = _$
(b) $C_S = _ X 8.34 \times 60 \times 1 = _$ Btu/(hr · σF)
(c) Heat exchanger effectiveness = _
(d) $x = \frac{C_c}{c_S C_{min}} = (_)(_) = _$
(e) $y = \frac{A_C F_R U_L}{C_c} = (_)(_) = _$

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10. Incident angle modifier (a) $F_R(\overline{\tau \alpha}) = F_R(\tau \alpha)_n \times 0.91$ (for two cover plates) $= _ x \ 0.91 = _$ (b) $F_R(\overline{\tau \alpha}) = F_R(\tau \alpha)_n \times 0.93$ (for one cover plate) $= _ x \ 0.93 = _$ 11. (a) $F_R^{'\overline{\tau \alpha}} = \frac{1}{1100 \ 100$

List c_1 , c_2 , A_S , A_D , Z from Table 11-5

12.
$$A_{S} \text{ or } A_{D} = _$$
 $Z = _$ $c_{1} = _$ $c_{2} = _$

For Solar Heating and DHW Systems:

13.
$$A_{50} = \frac{A_{S}(UA)_{L}}{F_{R}^{\tau\alpha} - F_{R}U_{L}(Z)}$$

 $A_{50} = \frac{(--)}{(--)} - (--)(--)} = ----- ft^{2}$

14.
$$A_c/A_{50} = _ = _$$

15. $\log_e(A_c/A_{50}) = _$
16. $F = c_1 + c_2 \log_e(A/A_{50})$
 $= _ + (_)(_) = _$
17. $A_c/A_{50} = 300/259 = 1.16$
18. $\log_e(A_c/A_{50}) = 0.15$
19. $F = _ + (_)(_) = _$

SOLAR SYSTEM DATA

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Building (Dwner	
Address		Ph
Contracto	r	Ph
Type of S	ystem (liquid or air, H/DHW	
Site and	Building Data	
1.	Location: Nearest City	Latitude
2.	Building UA	Btu/(hr•°F)
3.	DHW volume per day	gallons/day
4.	Collector manufacturer	
5.	Collector area	ft²
6.	Collector tilt	degrees
7.	Tilt = latitude +	degrees
8.	Collector orientation degrees	sfrom south
9.	Collector shading	% in December
10.	Collector efficiency data	
	(a) $F_{R}(\tau \alpha)_{n}$	
	(b) F _R UL	Btu/(hr•ft ² •°F)
	(c) Fluid temperature basis (circle	one)
	Case 1 T _i	
	Case 2 $\frac{T_i + T_{out}}{2}$	
	Case 3 Tout	
11.	Collector Fluid:	
	(a) Composition:	
	(b) Specific heat, c _p	Btu/(1b•°F)
	(c) Specific weight Y	lb/gal or lb/ft ³
	(d) Flow rate G	gal/min or ft ³ /min
Storage D	ata	
12.	Storage medium	
13.	Unit volume	gal/ft ² or ft ³ /ft ²
14.	Total volume (item 5 x 13)	gal or ft ³

		Worksheet A Sheet 2 c? 2 LIQUID SYSTEMS
15	. Specific heat of storage material c _n	Btu/(lb•°F)
16	. Specific weight	lb/gal or lb/ft ³
17	. Total mass (14 x 16) M	1b.
18	. Total heat capacity (17 x 15) ^C s = Mc _p	Btu/°F
19	. Total heat capacity per unit collector area (18 ÷ 5)	Btu/(ft²•°F)
Heat Ex	changers	
20	. Collector/storage type manufacturer	and
21	. Storage loop flow rate	gal/min, ft ³ /min
22	. Heat exchange effectiveness ε_{cs}	
23	. Load heat exchanger type	and
	manufacturer	
24	. Load loop flow rate	gal/min
25	. Building air supply flow rate	ft ³ /min
26	. Heat exchange effectiveness $\epsilon_{\rm L}$	
DHW Pre	heater	
27	 Collector/storage heat exchanger type manufacturer 	and
28	. Collector loop flow rate	gal/min, ft ³ /min
29	. Heat exchanger effectiveness $\epsilon_{H_{ij}}$	
30). Storage volume	gal
31	. Storage mass, M _{St.} (line 30 x 8.34)	1b
Auxilia	ry Furnace/Boiler	
34	Nanufacturan	
3	Bated capacity	Btu/br
21	Auxiliary energy source	Douy m
Auxilia	ary DHW Unit	a a]
30	. SIZE	ya i
3	Auxiliary energy source	0 Г
3	s. Hot water set temperature	- r

Worksheet B LIQUID SYSTEMS

	1	2		3	4	5	6	7
Month	Monthly Degree Days DD °F∙days	Monthly Space Htg Load Q _S Btu/Mo.	No. of Days/ Mo. N	Vol. of DHW Used/Mo. Gal./Mo.	Temp. Water Main Sup T _m °F	DHW Temp. Rise T _{HW} -T _m °F	Monthly DHW Load Q _W Btu/Mo.	Total Heating Load L Btu/Mo.
Jan.			31					
Feb.			28					
March			31					
April			30					
May	÷.		31					
June			- 30					
July			31					
Aug.			31					
Sept.			30					
Oct.			31					
Nov.			30					
Dec.			31	Ð				
						Total		

HEATING AND/OR DOMESTIC HOT WATER LOAD, L

Q_d = Btu/h

Project _____

(Given data or calculate as in Module 3)

 $DTD = 70 - T_0$

= 70 - =

Where: $T_0 = 99\%$ winter design temperature. (From ASHRAE Fundamentals, or Table 3-2)

70°F = indoor design

 $UA = \frac{Q_d}{DTD} =$

T_{HW} =

1. From Table 3-2 or Figures 3-2 through 3-13
2. Q_s = (24)(UA)(Degree Day)

3. (Vol/day)x(no. days/mo.) =4. From Table 8-3 for selected cities 6. $Q_w = (vol. of water) \times 8.34 \times 1 \times (T_{HW}^{-T}).$ _(gal./day)x(no. days/mo.)

7. L = $Q_{s} + Q_{w}$

TOTAL MONTHLY SOLAR RADIATION AVAILABLE, S

Project	
Location	
Collector Tilt	
Nearest Data Site	

	1	2	3	
Month	Monthly Avg. Daily Rad. on Tilt Surf. ^I T Btu/(Day•ft ²)	No. of Days in month N	Tot. Monthly Radiation on Tilt Surf. S Btu/(Mo•ft ²)	
Jan.		31		
Feb.		28		
March		31		
April		30		
May		31		
June		30		
July		31		
Aug.		31		
Sept.		30		
Oct.		31		
Nov.		30		
Dec.		31		

[1] From Table 5-5 for Colorado cities

[3] Column [1] x Column [2]

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Worksheet D Sheet 1 of 2 LIQUID SYSTEMS

COLLECTOR COMBINED PERFORMANCE CHARACTERISTICS, $F'_{R}(\tau \alpha) \cdot F'_{R}U_{I}$ PROJECT Collector Efficiency Data from Worksheet A (lines 10(a), (b)) Intercept, $F_{p}(\tau \alpha)_{n}$ 1. = Slope, F_RUL 2. 2. Slope, $F_R U_L = \frac{t_{in} + t_{out}}{2}$, 3. t_{out} = _____ ft² 3. Collector area, A 4. Collector volumetric flow rate (Worksheet A, 11(d)) _____ gal/min or ft³/min Correction to t_{in} basis Case 1: (no correction) $F_R(\tau \alpha)_n =$ 5. F_R U_L = _____ 6. Case 2: $F_R(\tau \alpha)_n = F_R \tau \alpha \times \left[\frac{1}{1 + \frac{F_R U_L A_c}{2 C_n}}\right] =$ $F_{R}U_{L} = F_{R}U_{L} \times \left[\frac{1}{1 + \frac{F_{R}U_{L}A_{c}}{2C}}\right] = - C_{c} = \dot{m}c_{p} = (volumetric)(density)(time)(specific)(heat)$ where: for liquids, density - (8.34 lb/gal) x (specific) for air, density = 0.075 lb/ft³ at 70° and 1 atm. specific heat = 0.24 Btu/1b.°F 7. Case 3: $F_R(\tau\alpha)_n = F_R(\tau\alpha)_n \times \left[\frac{1}{1 + \frac{F_R U_L A_c}{C}}\right] =$ $F_R U_L = F_R U_L \times \left[\frac{1}{1 + \frac{F_R U_L A_c}{C}}\right] = -$ Incident Angle Modifier, $\frac{F_R(\tau \alpha)}{F_R(\tau \alpha)_n} = \{.91, \text{ for two cover plates}, \text{ for one cover plate}\}$ 8.

Worksheet D Sheet 2 of 2 LIQUID SYSTEMS

Collector Loop Heat Exchanger Modifier,
$$\frac{F_R}{F_R}$$

9. For air systems and liquid systems without a collector/storage heat exchanger, $\frac{F_R'}{F_R} = 1$ Capacitance Rate:

10.
$$C_c = (\text{from line 6}) = ______Btu/(hr \cdot ^F)$$

11. $C_s = (\text{calc. as for } C_c \text{ above}) = _____Btu/(hr \cdot ^F)$
12. $C_s = (\text{lesser of } C_c \text{ of } C_c) = ____Btu/(hr \cdot ^F)$

$$\lim_{t \to \infty} \frac{1}{2} \lim_{t \to \infty}$$

13. Collector Storage Heat Exchanger Effectiveness, ϵ_{cs} = _____

14.
$$x = \frac{C_c}{c_s C_{min}} = \frac{1}{(\text{from Worksheet A, line 22})} = \frac{1}{(\text{from Worksheet A, line 22})}$$

15.
$$y = \frac{A_c(F_R U_L)}{C_c} = _ = _$$

16. $\frac{F_R'}{F_R} = \text{ from Figure 9-7 or } = \frac{1}{1 + y(x-1)} = _$

17.
$$F_{R}^{i}(\tau \alpha) = F_{R}(\tau \alpha)_{n} \times \frac{i\alpha}{(\tau \alpha)_{n}} \times \frac{i\alpha}{F_{R}} =$$

18. $F_{R}^{i}U_{L} = F_{R}U_{L} \times \frac{F_{R}^{i}}{F_{R}} =$

Worksheet E LIQUID SYSTEMS

CORRECTION FACTORS, K₂, K₄

		PROJECT	
Stora	age Ma	ass Capacitance Factor K ₂	
	Note	: M includes hot water sotrage volume where it is so heated	lar
	1.	gals/ft ² of collector	
	2.	K ₂ = (from Figure 9-8) =	<u> </u>
Load	Heat	Exchange Factor, K ₄	
	3.	ϵ_{L} (from Worksheet A, line 26) =	
	4.	$C_{hot water supply loop} = \dot{m}c_p = C_H$ (from Worksheet A, lines 24 x 8.25 x 60) =	
			Btu/(hr•ft ²)
	5.	$C_{air loop} = m_{p} = C_{A}$ (from Worksheet A, line 25 x 0.075 x .24 x 60) =	
			Btu/(hr•ft ²)
	6.	C _{min} = smaller of C _H or C _A =	Btu/(hr•ft ²)
	7.	(UA) bldg = (from Worksheet A, or B) =	
			Btu/(hr•°F)
	8.	<u>UA</u> =	
	9.	K ₄ = (from Figure 9-9) =	



SYSTEM PERFORMANCE PARAMETERS X, Y

PROJECT

	1	2	- 3	4	5	6	7	8
Month	Tot. Monthly Radiation on Tilt Surf. S Btu/(Mo•ft ²)	Total Heating Load L Btu/Mo.	S/L	۲ F ₁ •[3]	Mo. Av. Temp. Ta°F	212-T °Fa	Tot. llrs in Mo. ∆ time hr.	X
Jan.							744	
Feb.							672	
March							744	
April					14		720	
May							744	
June							720	
July							744	
Aug.							744	
Sept.							720	
Oct.							744	
Nov.							720	
Dec.							744	
1. From Workshe 2. From Workshe 4. $Y = \frac{A_c F_R'(\tau \alpha)}{L}$ 5. From Table 5 8. $X = \frac{A_c F_R'U_L(\tau \alpha)}{L}$ $= F_2 \cdot \{ [6] \cdot co \}$	et C, Col. 3 et B, Col. 7 $S \times K_4 = F_1 \cdot \frac{S}{L}$ -5 $\frac{ref - T_a)\Delta time}{L} \times K_2$ $[7]\} \div [2]$ Tumns			$ \begin{array}{c} A_{c} \\ F_{R} \\ \overline{\tau \alpha} \\ F_{R} \\ U_{L} \\ K_{1} \\ K_{2} \\ K_{4} \\ F_{1} = F_{2} \\ \end{array} $	$=$ $=$ $=$ $=$ $A_{c}F_{R}^{T} \overline{\tau \alpha} K_{4} =$ $A_{c}F_{R}^{T} U_{l} K_{2} =$			ft ² (Wksht D) (Wksht D) (Wksht E) (Wksht E) (Wksht E)



		Thinker 1					
	P			PROJECT			
	1	2	3	4	5	COLLECTOR AREA	ft ²
Month	Tot. Mo. Htg. Load L Btu/mo.	System Parameters X	System Parameters Y	Solar Fraction/ mo. f	Actual Solar en/mo E Btu/mo.		
Jan.							
Feb.							
March							
April							
May							
June							
July							
Aug.							
Sept.	-						
Oct.							
Nov.							
Dec.							

FRACTION OF TOTAL HEATING LOAD SUPPLIED BY SOLAR ENERGY, FAnnual

L_{tot} =

E_{tot} =

Etot F_{Annual} = Ltot

- From Worksheet B
 From Worksheet F, Column 9
 From Worksheet F, Column 4
 From "f chart", Figure 9-6
 E = f x L

Relative Areas Methods Worksheets Sheet 1 of 3

SOLAR SYSTEM DATA

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Build	ling C	lwner	
Addre	255		Ph
Contr	ractor		Ph
Туре	of Sy	vstem (liquid, air, H/DHW, DWH)	2
Site	and E	Building Data	
	1. 2. 3.	Location: Nearest City Building UA DHW volume per day	_Latitude Btu/(hr•°F) _gallons/day
Colle	ector	Data	
	4. 5. 6.	Collector manufacturer Collector Area, $A_c =Collector efficiency data from manufacturer's(a) F_R(\tau \alpha)$	_ft ² information:
		(b) F _R U _L	_Btu/(hr•ft ² •°F)
	7.	Correction for fluid temperature basis (a) Case 1: (no correction) (i) $F_R(\tau\alpha)_n = F_R\tau\alpha$ (from line 6) (ii) $F_RU_L = F_RU_L$ (from line 6) (b) Case 2: $\frac{T_{in} + T_{out}}{2}$ (correction needed)	Btu/(hr•ft ² •°F)
		$C_{c} = (\hat{m}c_{p})_{c} = (\hat{m}c_{rate})(density)(c_{rate})$	conversion ^(spectric)
		= <u>gal</u> x <u>lb</u> x 60 <u>min</u> min x <u></u> gal x 60 <u>h</u> r	x <u>Btu</u> Ib•°F Btu/(hr•°F)



Corrections to Collector Parameters

- 10. Incident angle modifier
- (a) $F_{R}(\bar{\tau}\alpha) = F_{R}(\tau\alpha)_{n} \times 0.91$ (for two cover plates) $= _ x \ 0.91 = _ ...$ (b) $F_{R}(\bar{\tau}\alpha) = F_{R}(\tau\alpha)_{n} \times 0.93$ (for one cover plate) $= _ x \ 0.93 = _ ...$ 11. (a) $F_{R}^{\dagger}\bar{\tau}\alpha = \frac{1 \text{ ine 10a or 10b } \times \frac{1 \text{ ine 8 or 9f}}{1 \text{ ine 8 or 9f}} = _ ...$ (b) $F_{R}^{\dagger}U_{L} = \frac{1 \text{ ine 7a(ii)}}{1 \text{ or 7b(ii)}} \times \frac{1 \text{ ine 8 or 9f}}{1 \text{ ine 8 or 9f}} = _ ...$ Btu/(hr.°F)

List c_1 , c_2 , A_S , A_D , Z from Table 11-5

12.
$$A_{S} \text{ or } A_{D} = _$$
 $Z = _$ $c_{1} = _$ $c_{2} = _$

For Solar Heating and DHW Systems:

18.
$$Log_e(A_c/A_{50}) = 0.15$$

19. F = + ()() =